

Effect of Presence of Other Heavy Metals on Removal of Cadmium by Low Cost Adsorbents

Dr. Sunil Jayant Kulkarni¹,

¹(Chemical Engineering Department, Datta Meghe College of Engineering, Airoli, Navi Mumbai, Maharashtra, India)

Abstract: Continuous packed column adsorption experimentations are generally carried out to optimize parameters like flow rates, bed height, initial concentration. Also studies on break through curves are integral part of all these investigations. Modeling for break through curve includes model fitting for Adam Bohart, Yoon Nelson and Thomas models. Estimation of efficiency, breakthrough point and exhaustion point is integral part of packed bed experimentation. It is important to study multicomponent adsorption to closely resemble the study to actual conditions. The current investigation focuses on multicomponent (binary) adsorption of cadmium with chromium and nickel. Investigation is aimed at studying the effect of various concentrations of other heavy metal on cadmium removal by using groundnut shell derived activated carbon (GNSA) and rice husk derived activated carbon (RHA). Ionic radius affected selectivity of adsorbate. Studies reveal that cadmium was most preferred adsorbate as it had higher ionic radius than nickel and cadmium.

Keywords: Adsorption, adsorbate, removal, concentration, pH.

I. INTRODUCTION

Removal of heavy metal from synthetic effluent is widely discussed and investigated research domain. There is huge scope for research since different waste materials can be used with different activation methods [1-4]. Also use of various contacting pattern is widely studied [5-8]. Investigation on adsorption is generally carried out conventionally in three parts. The batch adsorption study includes batch experimentation for finding isotherm and kinetic parameters [9-12]. The parameters like pH, initial concentration, contact time, particle size are studied in most of these studies. Continuous experimentation is carried generally to optimize parameters like flow rates, bed height, initial concentration. Also studies on break through curves are integral part of all these investigations [13-18]. Modeling for break through curve includes model fitting for Adam Bohart, Yoon Nelson and Thomas models. Estimation of efficiency, breakthrough point and exhaustion point is integral part of packed bed experimentation [19-25]. Industrial effluent contains more than one metal. It is important to study multi component adsorption to closely resemble the study to actual conditions. Author has, in past carried out investigation on synthetic effluent with single component [18,26]. The current investigation focuses on multicomponent (binary) adsorption of cadmium with chromium and nickel. Investigation is aimed at studying the effect of various concentration of other heavy metal on cadmium removal by using groundnut shell derived activated carbon (GNSA) and rice husk derived activated carbon (RHA).

II. LITERATURE REVIEW

An investigation on competitive sorption of Cd, Cu, Pb and Zn was carried out by Ramsenthil and Meyyappan [29]. According to these studies; there exist a competitive adsorption for the binary mixture solution. Langmuir and Freundlich model in the applied concentration ranges were adequate to describe the uptake. Shaken et.al. used Zeolite for competitive adsorption of heavy metals [30]. In their investigation, they determined percentage sorption and distribution coefficients. They found that Freundlich model described the sorption of metals satisfactorily. Adsorption and distribution coefficient followed the trend $Pb > Cu > Zn > Cd > Ni$. They found that Cu was better adsorbed metal of the two. Al-Malack et.al. investigated competitive adsorption of lead and cadmium [31]. Municipal organic solid waste derived activated carbon was used by them. Factors affecting adsorption such as pH, contact time, metal concentration and adsorbent dosage were also studied by them. Studies revealed that, non-linear Freundlich adsorption isotherm and pseudo-second-order kinetic models described the uptake of both the metals. An investigation on sorption of heavy metals was carried out by Singh and Gupta [32]. According to them, most of the investigations included the isotherm and kinetics of metal uptake. An investigation on competitive sorption of Cd, Cu, Pb and Zn was carried out by Zemanova et.al. [33]. Three types of soils were used by them, aGleyicFluvisol, a GleyicCambisol, and a Chernozem. They found that sorption from single-metal solution was more effective than sorption under multi-metal conditions. According to study carried out by Futalanet.al., forcopper, nickel and lead adsorption on chitosan-immobilized on bentonite, the adsorption followed pseudo second order kinetics[34]. Also they found

that, nickel removal followed Langmuir model while other two metals followed Freundlich equation. Rashid et.al investigated uptake of Cadmium (Cd) and Lead (Pb) and their subsequent accumulation in edible tissue of plant[35]. According to them, phytoaccumulation and adsorption of Cd was higher than Pb and copper. An investigation was carried out by Apiratikul et.al. on biosorption of binary mixtures of heavy metals[36]. Their emphasis was green macro alga, *Caulerpalentillifera*. Experiments were carried out in order to study sorption potential of metals. Their results indicated that binary adsorption was competitive in nature and the adsorption capacity for any single metal decreased by 10-40% in the presence of the others.

III. METHODOLOGY

The adsorbents were prepared by thermal activation preceded by some chemical treatment for the raw material as explained in the earlier work [8,15,19] by the author. The standard solutions of cadmium, nickel and chromium were prepared by taking appropriate amount of cadmium sulphate, nickel sulphate and potassium dichromate as in case of single component batch and column experiments [8,15,19,27]. The appropriate samples were prepared from stock solutions. 100 ml of the samples were contacted with 3 grams of adsorbents at 6 pH and the samples were analyzed after 15-30 minutes intervals. Standard spectrophotometric methods were used for analysis.

IV. RESULT AND DISCUSSION

4.1 Effect of nickel on cadmium removal for GNSA

To study the effect of presence of nickel on cadmium removal, to 100 mg per liter cadmium effluent, nickel was added. Four samples were prepared by using cadmium sulphate and nickel sulphate. The four samples had 10, 20, 30 and 40 mg/l of nickel and 100 mg/l of cadmium each. The batch experiments were performed in the same way as explained in the batch experimental methodology. Optimum values of the pH, adsorbent dose were used. It was observed that with addition of nickel, the cadmium removal dropped marginally. The maximum removal decreased from 68 to 65 percent for addition of 10 mg/l of Ni. For contact time of 15 minutes the loss of percentage removal was 1.2 percent, which increased to 3 percent of 180 minutes. The drop in the cadmium removal was very small. Studies reveal that cadmium had higher ionic radius and hence it is preferred over nickel by the adsorbent. Fig.1 depicts the effect of nickel on cadmium removal. The final removal at equilibrium, was 68 percent without Ni, 65 for 10 mg/l of Ni, 64 for 20 mg/l Ni, 63.1 for 30 mg/l Ni and 62.3 for 40 mg/l of Ni. [

Table 1: Cd removal at various Ni concentrations for GNSA

Time/Ni mg/l	% Cd Removal				
	0	10	20	30	40
Minutes					
15	26	24.8	23	22	21.3
30	36	28.5	27	26	25
60	46	40	38.5	37.5	36.5
90	51	49.8	48.3	47.3	46.3
120	54	52	50.5	49.5	48.5
150	56.5	55.6	54.1	53.1	52.1
180	68	65	64	63.1	62.3

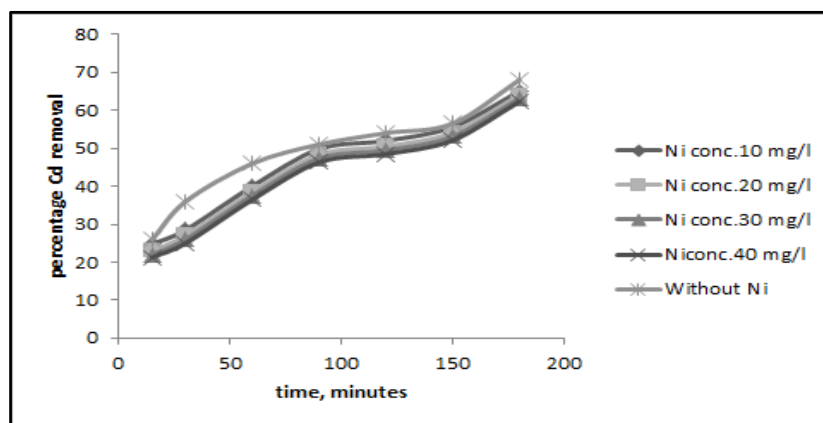


Fig.1 Effect of nickel on cadmium removal for GNSA

4.2 Effect of chromium on cadmium removal for GNSA

Effect of presence of chromium on cadmium removal is shown in Fig. 2 for GNSA adsorbent. For 10 mg/l concentration of chromium, initial 2.2 percent reduction decreases to 1 percent after 180 minutes. The percentage removal at equilibrium was 68 percent without Cr, which reduced to 67, 65.5, 66 and 67 percent respectively for addition of 10, 20, 30 and 40 mg/l of Cr. This indicates that cadmium is most preferred heavy metal for the adsorbent out of these three heavy metals

Table 2 : Cd removal at various Cr concentrations for GNSA

Time/Cr Concentration	% Cd Removal				
	0	10	20	30	40
mg/l					
minutes					
15	16	13.8	12.3	11.05	10.05
30	36	26	24.5	23.5	22.5
60	46	39.5	38.5	37.5	37.3
90	51	47.1	45.6	44.6	43.6
120	54	47.5	46	45	44
150	56.5	53.8	53.3	53	52
180	68	67	65.5	66	67

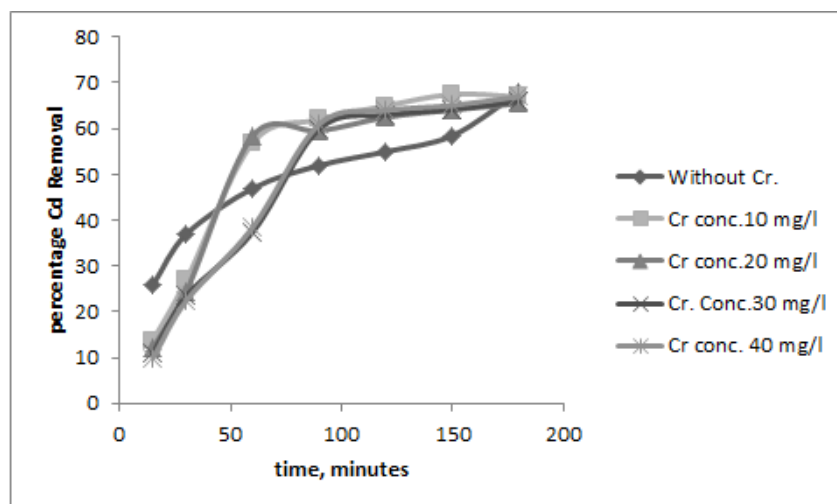


Fig 2: Effect of chromium on cadmium removal for GNSA

4.3 Effect of presence of nickel on cadmium removal for RHA

Effect of presence of nickel on cadmium removal is shown in Fig. 3 for RHA adsorbent. The experimental data reveal that the presence of nickel has slightly more effect than chromium. For 10 mg/l concentration of nickel initial 2.4 percent reduction at 30 minutes increases to 5.6 percent for 180 minutes. The percentage removal at equilibrium was 79 percent without nickel, which reduced to 73.4, 73.2, 71 and 69.1 percent respectively for addition of 10, 20, 30 and 40 mg/l of Ni. This indicates that Cadmium is most preferred heavy metal for the adsorbent out of these three heavy metals.

Table:3: Cd removal at various Ni concentrations for RHA

Time/Ni Concentration	% Cd Removal				
	0	10	20	30	40
mg/l					
minutes					
30	30.6	27	26	25.5	25.6
60	43.6	40	38	48.3	45.9
90	58.1	55	52	57	57.1

120	74.2	70	67	65	64.6
180	79	73.4	73.2	71	69.1

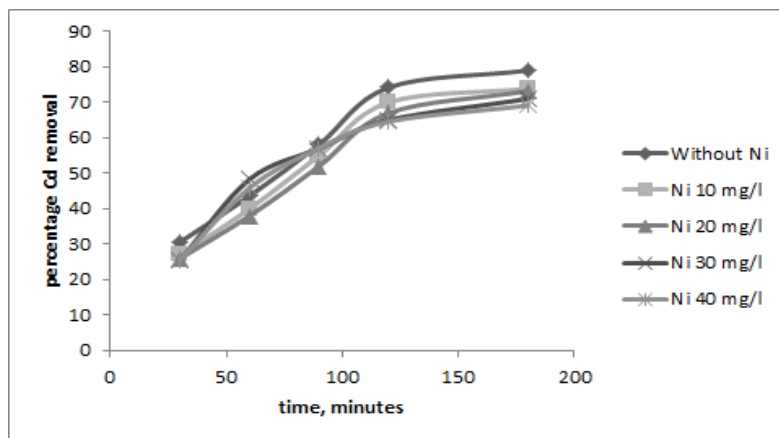


Fig.3: Effect of nickel on cadmium removal for RHA

4.4 Effect of chromium on cadmium removal for RHA

To study the effect of presence of chromium on cadmium removal, to, 100 mg per liter cadmium effluent chromium was added. Four samples were prepared by using cadmium sulphate and potassium dichromate. The four samples had 10, 20, 30 and 40 mg/l of chromium and 100 mg/l of cadmium each. The batch experiments were performed in the same way as explained in the batch experimental methodology explained. Optimum values of the pH, adsorbent dose were used. It was observed that with addition of chromium, the cadmium removal dropped marginally. The maximum removal decreased from 79 to 78 percent for addition of 10 mg/l of Cr. For contact time of 30 minutes the loss of percentage removal was 0.6 percent, which increased to 1 percent of 180 minutes. The drop in the cadmium removal was very small. Studies reveal that cadmium had higher ionic radius and hence it is preferred over chromium by the adsorbent. Fig.4 depicts the effect of chromium on cadmium removal. The final removal at equilibrium, was 79 percent without Cr, 78 for 10 mg/l of Cr, 76 for 20 mg/l Cr, 70 for 30 mg/l Cr and 68.1 for 40 mg/l of Cr.

Table:4: Cd removal at various Cr concentrations for RHA

Time/Cr Concentration mg/l	% Cd Removal				
	0	10	20	30	40
minutes					
30	30.6	30	30	29	28.5
60	43.6	42.2	41	40	38.9
90	58.1	57	55	55	52
120	74.2	74	71	69	68
180	79	78	76	70	68.1

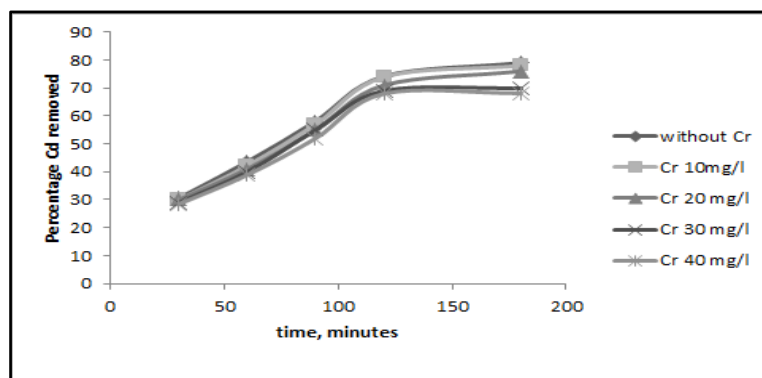


Fig.4: Effect of chromium on cadmium removal for RHA

V. CONCLUSION

For GNSA with Ni, the maximum removal decreased from 68 to 65 percent for addition of 10 mg/l of Cr. For contact time of 15 minutes the loss of percentage removal was 2.2 percent, which increased to 3 percent of 180 minutes. The drop in the cadmium removal was very small. Ionic radius affected selectivity of adsorbate. Studies reveal that cadmium had higher ionic radius. The experimental data reveal that the presence of Cr has negligible effect. For 10 mg/l concentration of Cr, initial 2.2 percent reduction drops to 1 percent after 180 minutes. For RHA, with chromium, the final removal at equilibrium, was 79 percent without Cr, 78 for 10 mg/l of Cr, 76 for 20 mg/l Cr, 70 for 30 mg/l Cr and 68.1 for 40 mg/l of Cr. For RHA, the experimental data reveal that the presence of nickel has slightly more effect than cadmium. For 10 mg/l concentration of nickel initial 2.4 percent reduction at 30 minutes increases to 5.6 percent for 180 minutes. The percentage removal at equilibrium was 79 percent without nickel, which reduced to 73.4, 73.2, 71 and 69.1 percent respectively for addition of 10, 20, 30 and 40 mg/l of Ni.

REFERENCES

- [1] H. ZavvarMousavi, S. R. Seyedi, Nettle ash as a low cost adsorbent for the removal of nickel and cadmium from wastewater, *Int. J. Environ. Sci. Tech*, 8(1), 2011, 195-202.
- [2] PairatKaewsarn, Qiming Yu, Cadmium(II) removal from aqueous solutions by pre-treated biomass of marine alga *Padina* sp., *Environmental Pollution*, 112, 2001, 209-213.
- [3] Ai- Min-Li, Hai-Suo Wu, Quan Zing Zang, Gen Cheng Zang, Cao Long, ZengHaoFei, FuQuang Liu, Jin Long Chen, Thermodynamic Study Of Adsorption Of Phenolic Compounds From Aqueous Solution By Water Compatible Hypercross Linked Polymeric Adsorbent, *Chemical Journal Of Polymeric Science*, 22(3), 2004, 239-267.
- [4] PallaviAmale, Sunil Kulkarni, KavitaKulkarni, A Review on Research for Industrial Wastewater Treatment with Special Emphasis on Distillery Effluent, *International Journal of Ethics in Engineering & Management Education*, 1(9), 2014, 1-4.
- [5] Kulkarni Sunil J, Tapre Ravi W., PatilSuhav V., Fluidized Bed Activated Carbon Adsorption For Removal Of Phenol From Wastewater, *Int. J. Res. Chem. Environ.*, 2(4), 2012, 101-106.
- [6] Zhu Li-Nan, Ma Jun, Yang Shi-Dong, Removal Of Phenol By Activated Alumina Bed In Pulsed High Voltage Electric Field, *Journal Of Environmental Sciences*, 21, 2007, 409-415.
- [7] PallaviAmale, Sunil Kulkarni, KavitaKulkarni, Studies on Packed Bed Treatment for Organic Matter in Distillery Effluent, *International Journal of Engineering Science and Innovative Technology*, 3(5), 2014, 268-272.
- [8] Sunil J. Kulkarni, Ravi W. Tapre, Mass Transfer Studies on Fluidized Bed Adsorption Column for Phenol Adsorption, *International Journal of Science and Research*, 2(12), 2013, 101-104.
- [9] C. O. Nweke, G. C. Okpokwasili, Removal of Phenol from Aqueous Solution by Adsorption onto Activated Carbon and Fungal Biomass, *International Journal of Biosciences*, 3(8), 2013, 11-21.
- [10] N. Ghasemi, M. Ghasemi, S. Mashhadi and M.H. Tarraf, Kinetics and Isotherms Studies for The Removal of Ni(II) From Aqueous Solutions Using Rosa Canina L, *International Congress on Informatics, Environment, Energy and Applications-IEEA 2012*, 38, IACSIT Press, Singapore.
- [11] S.J. Kulkarni, Dr.J.P. Kaware, Isotherm and Kinetics of Phenol Removal by Adsorption- A Review, *International Journal of Research* 1(8), 2014, 287-293.
- [12] I-Hsien Lee, Yu-Chung Kuan, Jia-Ming Chern, Equilibrium and kinetics of heavy metal ion exchange, *Journal of the Chinese Institute of Chemical Engineers*, 38, 2007, 71- 84.
- [13] Sunil J Kulkarni, Dr. Jayant P Kaware. Removal of Cadmium from Wastewater by Groundnut Shell Adsorbent-Batch and Column Studies, *International Journal of Chemical Engineering Research*, 6(1), 2014, 27- 37.
- [14] Zahra Saadi, ReyhaneSaadi and Reza Fazaeli, Fixed-bed adsorption dynamics of Pb (II) adsorption from aqueous solution using nanostructured γ -alumina, *Journal Of Nanostructure in Chemistry*, 3(1), 2013, 1-8.
- [15] Sunil J. Kulkarni, Jayant P. Kaware, Analysis of Packed Bed Adsorption Column with Low Cost Adsorbent for Cadmium Removal, *Int.J. of Thermal and Environmental Engineering*, 9(1), 2015, 17-24.
- [16] Olowoyo, D.N and Orherhe, O.M., Production Of Ion Exchange Resins From Sugar Cane Bagasse For The Adsorption Of Lead And Cadmium Ions From Aqueous Solution, *Journal of Research in Environmental Science and Toxicology*, 3(1), 2014, 1-5.
- [17] Kulkarni Sunil J., KawareJayant P., Batch and Column Studies for Phenol Removal from Wastewater Using Low Cost Adsorbent, *Int. J. Res. Chem. Environ.*, 4(3), 2014, 127-132.

- [18] S. J. Kulkarni and J. P. Kaware, Kinetics of Phenol Uptake from Wastewater by Adsorption in a Fixed Bed, *Journal of Chemical, Biological and Physical Sciences*, 4(4), 2014, 3116-3123.
- [19] Sunil J. Kulkarni, Jayant P. Kaware, Packed Bed Adsorption Column Modeling for Cadmium Removal, *Int. J. of Thermal and Environmental Engineering*, 9(2), 2015, 75-82.
- [20] S. J. Kulkarni and J. P. Kaware, Packed Bed Modeling for Adsorptive Removal of Phenol, *Journal of Chemical, Biological and Physical Sciences, Section A*; 5(2), 2015, 1146--1151.
- [21] J.T.Nwabanne,P.K.Igbokwe, Adsorption Performance of Packed Bed Column for the removal of Lead (ii) using oil Palm Fibre, *International Journal of Applied Science and Technology*, 2(5), 2012, 106-115.
- [22] Mckay,M.J. Gordon Bino, Fixed Bed Adsorption for the Removal of Pollutants from Water, *Environ. Pollute.*, 66, 1990, 33-53.
- [23] Sunil J. Kulkarni And Jayant P. Kaware, Modeling For Packed Bed Phenol Removal By Low Cost Adsorbent Prepared From Rice Husk, *Sci. Revs. Chem. Commun.*, 6(1), 2016, 1-11.
- [24] Sulaymon, Abbas Hamid, Abbood, DheyaaWajid, Ali and Ahmed Hassoon, Removal of Phenol and Lead from Synthetic Wastewater by Adsorption onto Granular Activated Carbon in Fixed Bed Adsorbers: Prediction of Breakthrough Curves, *Desalination and Water Treatment*, 40(1), 2012, 244.
- [25] H. D. S. S. Karunarathna and B. M. W. P. K. Amarasingha, Fixed Bed Adsorption Column Studies for the Removal of Aqueous Phenol from Activated Carbon Prepared from Sugarcane Bagasse, *Energy Procedia*, 34, 2013, 83-90.
- [26] Sunil J. Kulkarni, JayantPrabhakarKaware, Phenol removal from effluent by rice husk carbon: batch and column studies, *Int. J. Environmental Engineering*, 7(2), 2015,131-142.
- [27] Sunil J. Kulkarni, Jayant P. Kaware, Analysis of Packed Bed Adsorption Column with Low Cost Adsorbent for Cadmium Removal, *Int. J. of Thermal and Environmental Engineering*, 9(1), 2015, 17-24.
- [28] S. J. Kulkarni and J. P. Kaware, Kinetics of Phenol Uptake from Wastewater by Adsorption in a Fixed Bed, *Journal of Chemical, Biological and Physical Sciences*, 4(4), 2014, 3116-3123.
- [29] R.Ramsenthil and Rm.Meyyappan, Single and Multi-component Biosorption of Copper and Zinc Ions using Microalgal Resin, *International Journal of Environmental Science and Development*, 1(4), 2010, 298-301.
- [30] Sabry M. Shaheen, Aly S. Derbalah, andFarahat S. Moghannm, Removal of Heavy Metals from Aqueous Solution by Zeolite in Competitive Sorption System, *International Journal of Environmental Science and Development*, 3(4), 2012, 362-365.
- [31] Muhammad H. Al-Malack, Omar G. Al-Attas, Abdullah A. Basaleh, Competitive adsorption of Pb^{2+} and Cd^{2+} onto activated carbon produced from municipal organic solid waste, *Desalination and Water Treatment*, 60, 2017, 310–318.
- [32] Neeta Singh, Dr. S. K. Gupta, Adsorption of Heavy Metals: A Review, *International Journal of Innovative Research in Science, Engineering and Technology*, 5(2), 2016, 2267-2281.
- [33] VeronikaZemanová, LukášTrakal, PavlaOchecová, JiřinaSzáková and Daniela Pavlíková, A Model Experiment: Competitive Sorption of Cd, Cu, Pb and Zn by Three Different Soils, *Soil and Water Res.*, 9(3), 2014, 97–103.
- [34] Cybelle Morales Futalan, Wan-Chi Tsai, Shiow-Shyung Lin, Maria Lourdes Dalida and Meng-Wei, Copper, nickel and lead adsorption from aqueous solution using chitosan-immobilized on bentonite in a ternary system, *Sustain. Environ. Res.*, 22(6), 2012, 345-355.
- [35] Audil Rashid, Tariq Mahmood, Faisal Mehmood, Azeem Khalid, Beenish Saba, AniqBatoool, AmmaraRiaz, Phytoaccumulation, Competitive Adsorption And Evaluation Of Chelators-Metal Interaction In Lettuce Plant, *Environmental Engineering and Management Journal*, 13(10), 2014, 2583-2592.
- [36] RonbanchobApiratikul, Taha F. Marhaba, SuraphongWattanachira and PrasertPavasant, Biosorption of binary mixtures of heavy metals by green macro alga, *Caulerpalentillifera*, Songklanakarim, *J. Sci. Technol.*, 26 (Suppl. 1), 2004, 199-207.